

ACTIVE APPLICATION ORIENTED LEARNING OF COMPLEX DYNAMICAL SYSTEMS WITH APPLICATION TO MPC

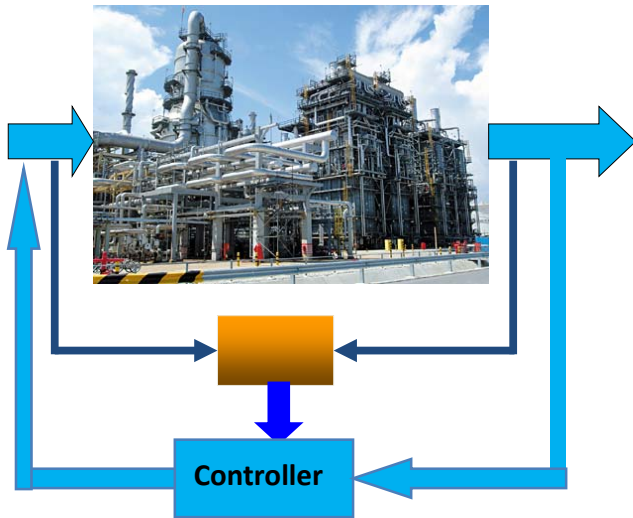
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AdBIOPRO - Center for Advanced Bioproduction
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DDCLS'18
May 26, 2018



The problem



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I'm afraid this still describes state-of-the art....

Outline

Application oriented experiment design

Output error models

The impact of optimal experiments on the identification problem

Computing the optimal input

Experimental results

Active application oriented learning

Application oriented dual control

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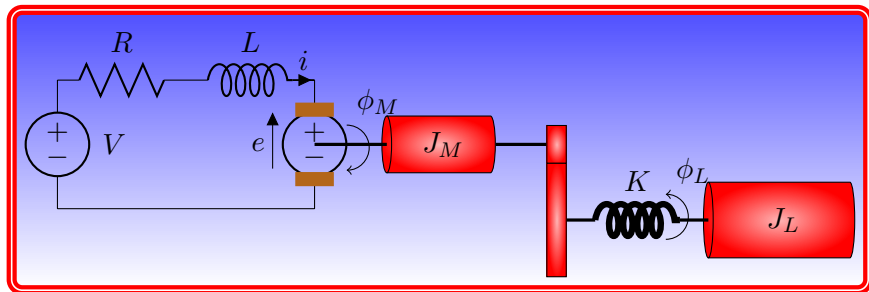
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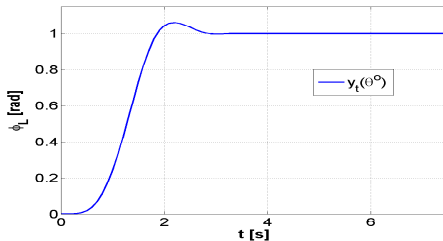
An application example: MPC of a DC-motor



- Input: Voltage V
- Output: Angle ϕ_L
- Model parameters θ : Resistance R , Moment of inertia J_L , Elasticity K , ...
- True parameters: θ_o

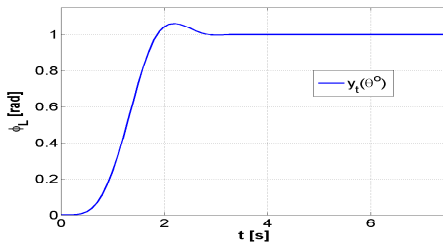
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- Ideal response: $y_t(\theta_o)$ - true parameters used in MPC



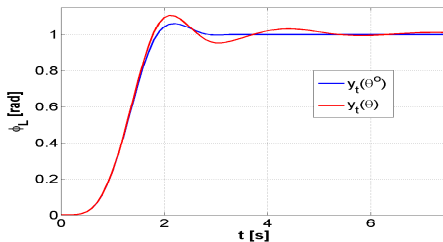
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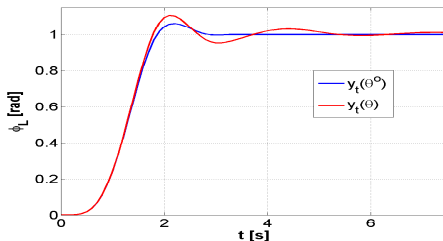
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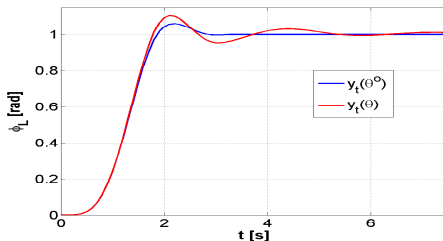


Performance degradation / Set of acceptable models

$$V_{\text{app}}(\theta) = \frac{1}{N} \sum_{t=1}^N (y_t(\theta_o) - y_t(\theta))^2$$

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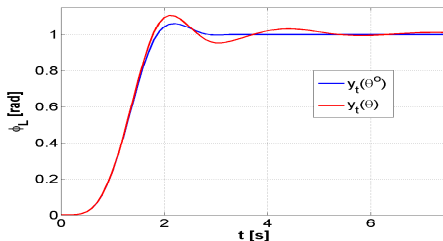
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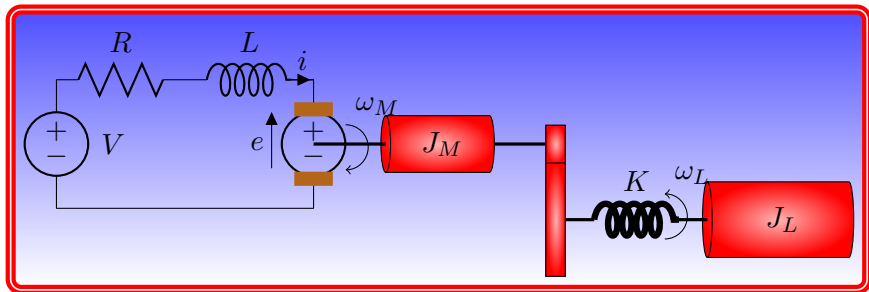


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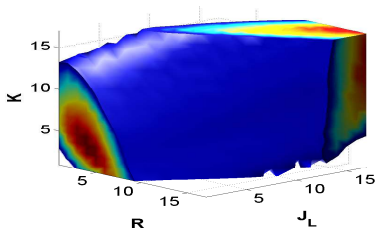
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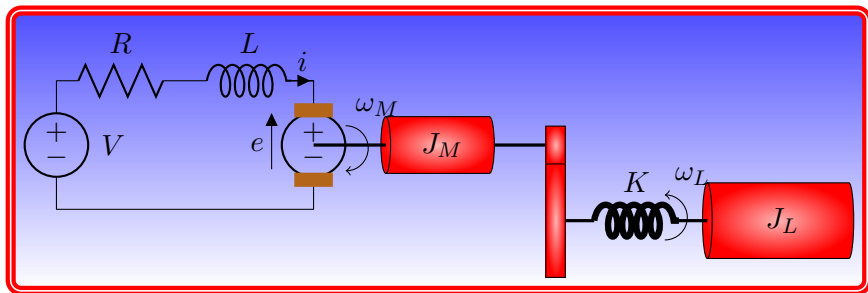
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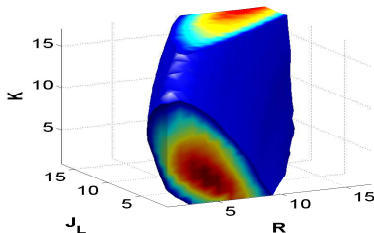
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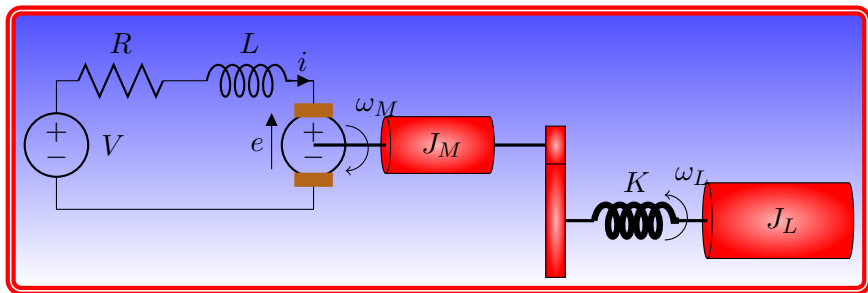
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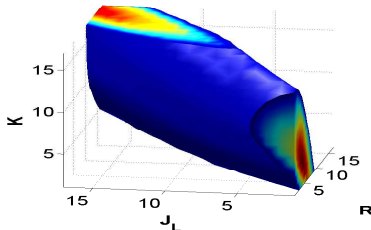
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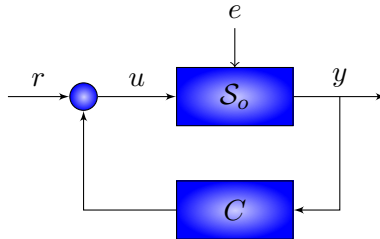
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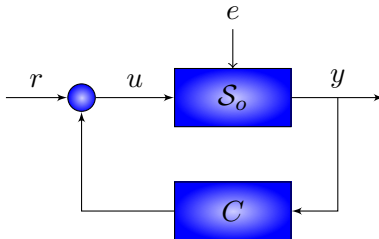
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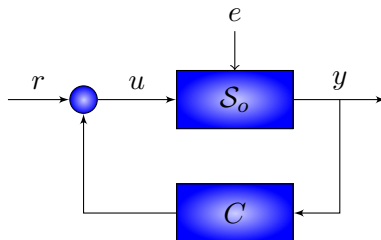
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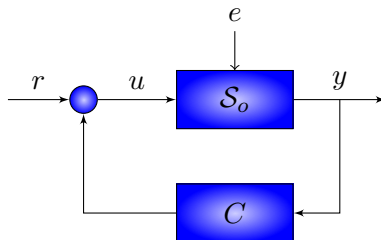
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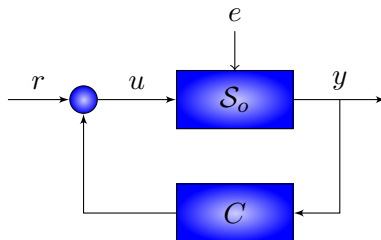
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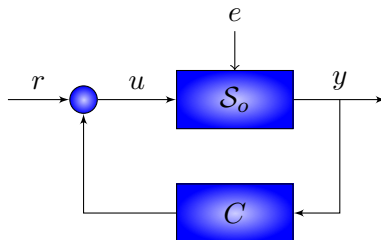
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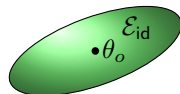
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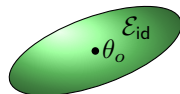
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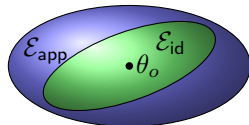
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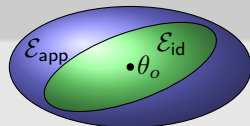
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$$\min \text{NE}[u_t^2]$$

$$\text{s.t. } \mathcal{E}_{\text{id}} \subseteq \mathcal{E}_{\text{app}} \subset \mathbb{R}^n$$



An alternative formulation

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can approximately be formulated as

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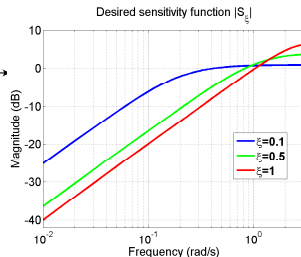
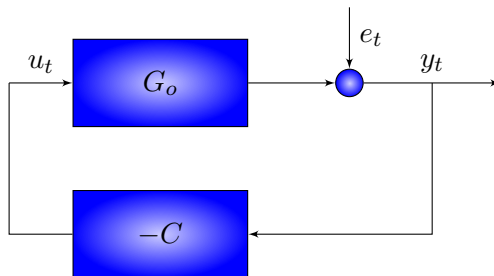
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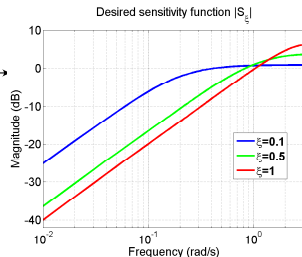
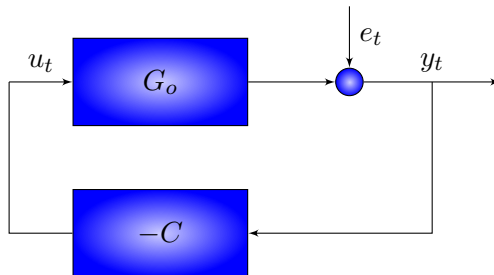
Identification cost matched to performance degradation

Model Reference Control



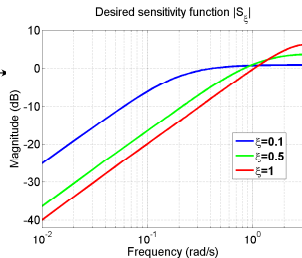
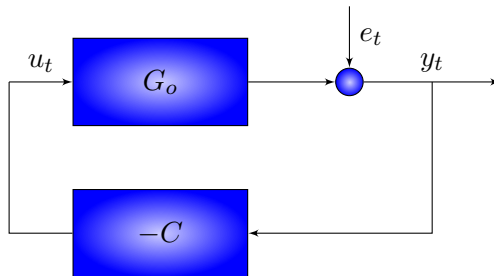
- Controller $C = C(G)$, G output error model

Model Reference Control



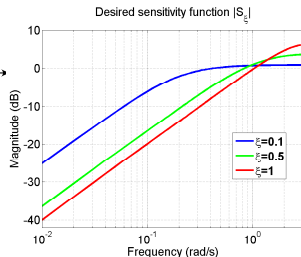
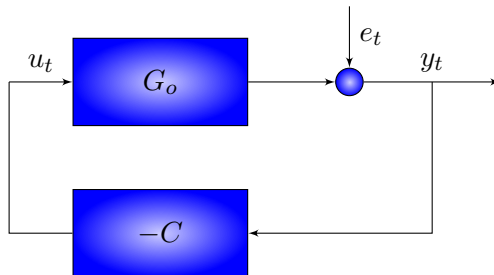
- Controller $C = C(G)$, G output error model
- Desired sensitivity function: S_ξ

Model Reference Control



- Controller $C = C(G)$, G output error model
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- Achieved sensitivity function: $S(G) = \frac{1}{1+C(G)G_o}$

Model Reference Control



- Controller $C = C(G)$, G output error model
- Desired sensitivity function: S_ξ
- Achieved sensitivity function: $S(G) = \frac{1}{1+C(G)G_o}$
- Performance degradation: $V_{\text{app}}(G) := \left\| \frac{S(G) - S_\xi}{S_\xi} \right\|_2^2$

Model Reference Control

$$\begin{aligned} \min & \text{NE}[u^2(t)] \\ \text{s.t. } & NV_{\text{id}}(\theta) \geq \gamma \lambda_e n V_{\text{app}}(\theta) \end{aligned}$$

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- Matching condition: $NV_{\text{id}}(\theta) = \gamma \lambda_e n V_{\text{app}}(\theta)$

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- *Experimental conditions during identification should be a scaled version of the desired operating conditions!*

Outline

Application oriented experiment design

Output error models

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Summary

Static gain estimation

$$y_t = \sum_{k=1}^n \theta_k u_{t-k} + e_t$$

Static gain estimation

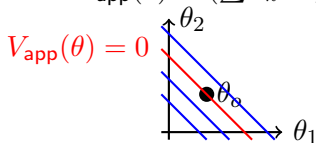
$$y_t = \sum_{k=1}^n \theta_k u_{t-k} + e_t$$

Performance degradation: $V_{\text{app}}(\theta) = (\sum \theta_k - \sum \theta_k^o)^2$

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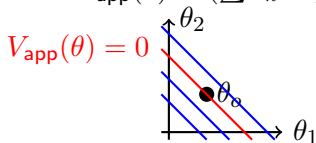
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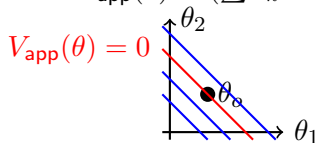
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Static gain estimation

Model order:	low	true	high
Accuracy:		<i>good</i>	

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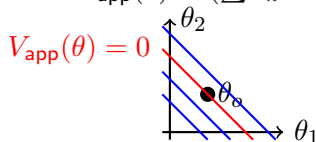
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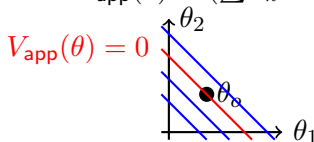
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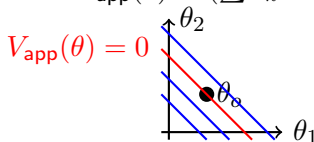
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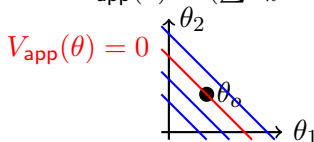
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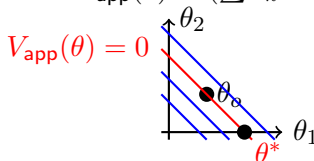
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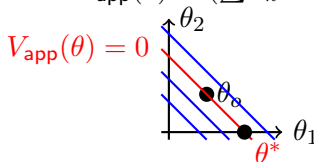
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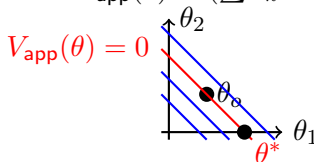
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Application oriented experiment design: Summary

Application oriented experiment design

Aims at achieving

$$N V_{\text{id}}(\theta) = \lambda_e \gamma n V_{\text{app}}(\theta)$$

using minimum energy

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 - ▶ Choice of model structure less critical

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Computations: The Information Application Inequality

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The Information Application Inequality

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The Information Application Inequality

Recall: V_{id} linear in the input spectrum

Information Application Inequality is an LMI in the input spectrum

Computations

$$\begin{array}{ll}\min & NE[u_t^2] \\ \text{s.t.} & \mathcal{I}_1^N \succeq \frac{\gamma n}{2} V''_{\text{app}}\end{array}$$

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Computations

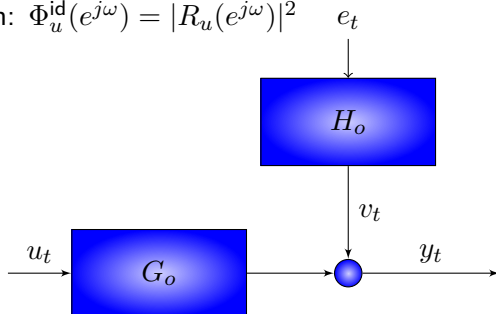
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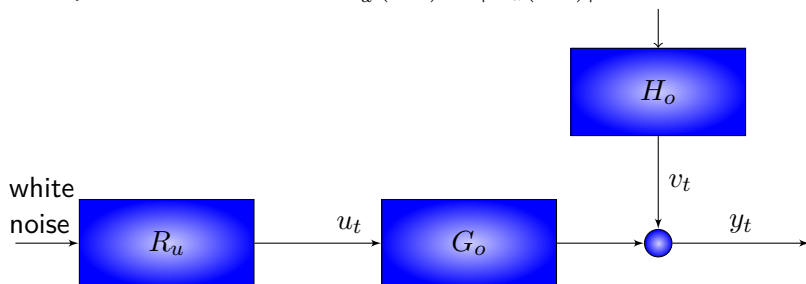
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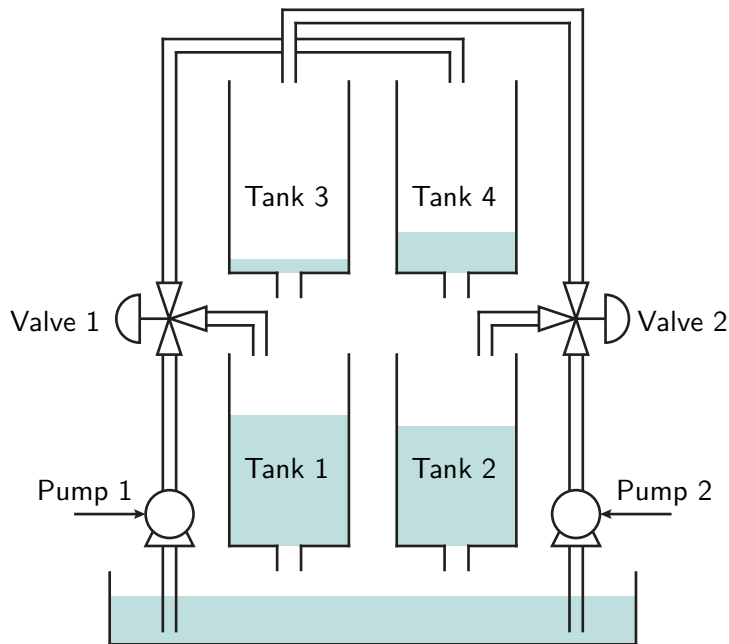
Experimental results

Active application oriented learning

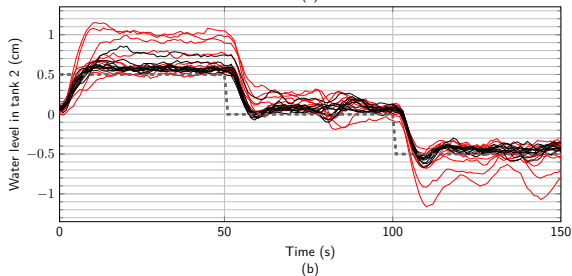
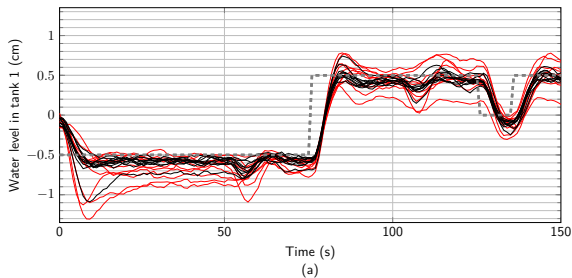
Application oriented dual control

Summary

Experimental results: Water tank process



Experimental results: Water tank process



MPC: Black: based on AOID-model. Red: based on white noise excitation

Application oriented experiment design

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(e.g. Rojas, Welsh, Goodwin, Feuer 2007)

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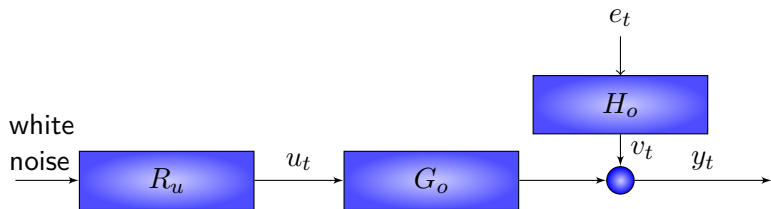
Experimental results

Active application oriented learning

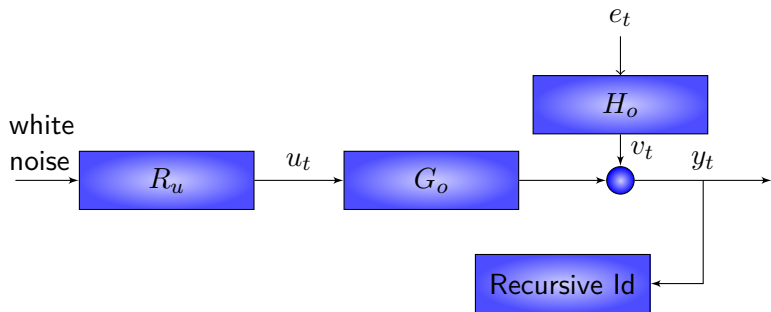
Application oriented dual control

Summary

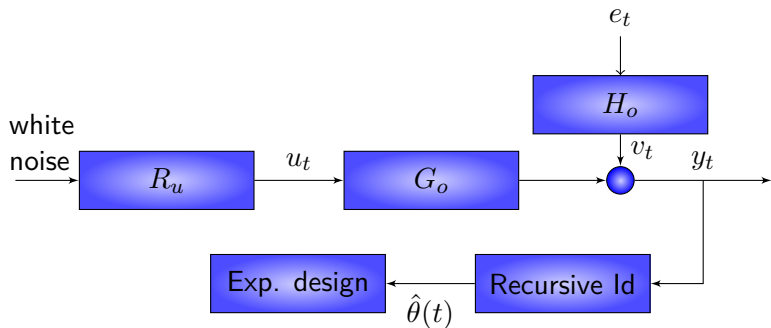
Active application oriented learning



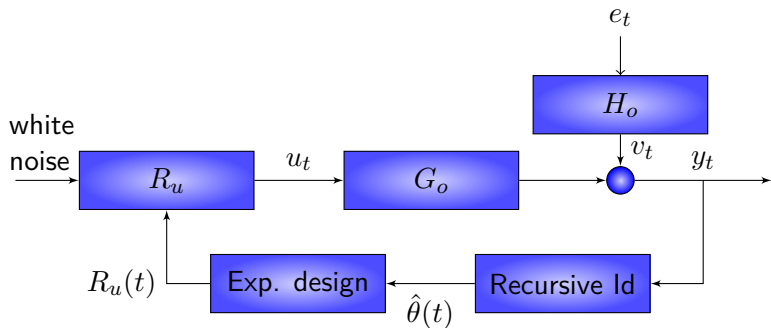
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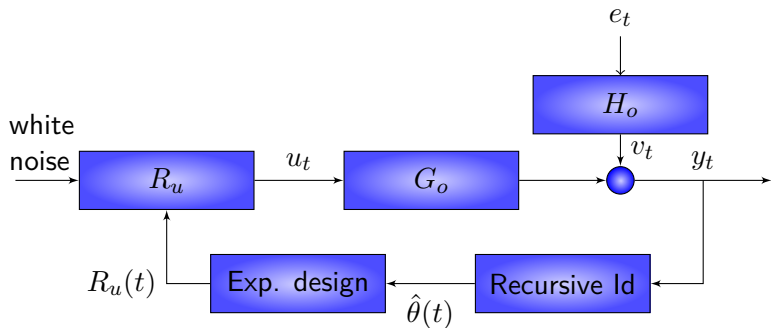
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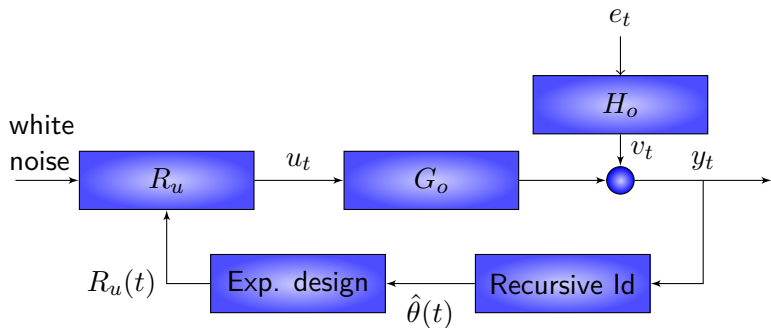


Active application oriented learning



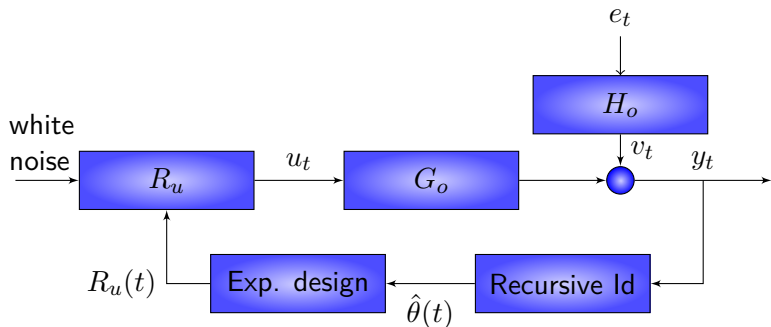
- An adaptive feedback system

Active application oriented learning



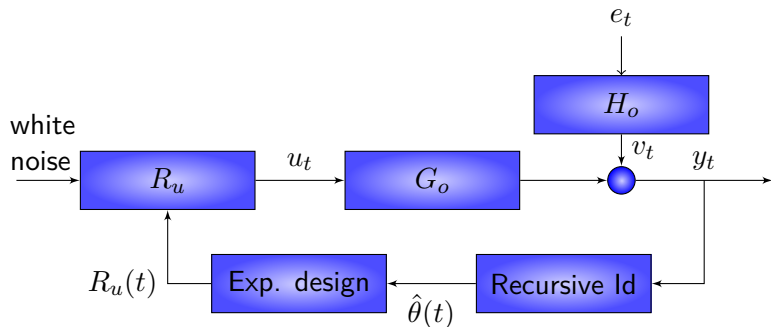
- An adaptive feedback system
- But measured signal not fed back directly

Active application oriented learning



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- Convergence?
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Theorem

- *True linear time-invariant system in the model set*
- *System stable*

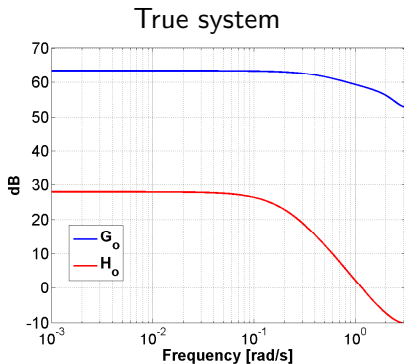
$\Rightarrow \hat{\theta}(t)$ *has the same asymptotic accuracy as the off-line estimate that uses data collected under the optimal experimental conditions (using knowledge of θ_o)*

Active application oriented learning

What happens when true system is not in the model set?

Example: Non-minimum phase zero estimation

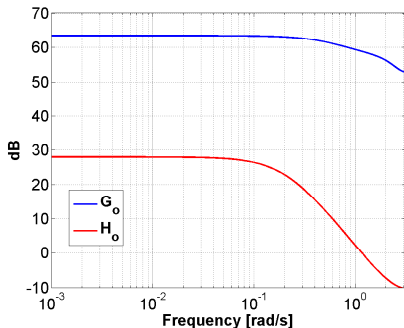
$$\text{True system: } y_t = \frac{(q - 3)(q - 0.1)(q - 0.2)(q + 0.3)}{q^4(q - 0.5)}u_t + \frac{q}{q - 0.8}e_t^o$$



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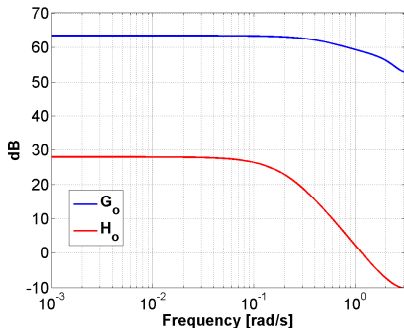


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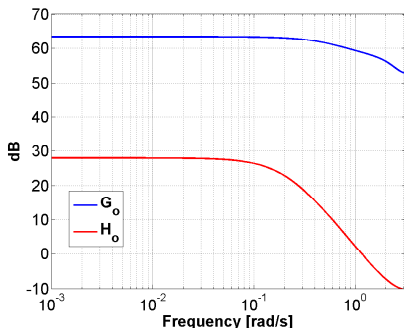


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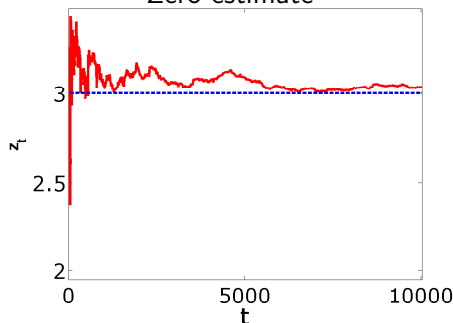
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Zero estimate



Outline

Application oriented experiment design

Output error models

The impact of optimal experiments on the identification problem

Computing the optimal input

Experimental results

Active application oriented learning

Application oriented dual control

Summary

Application oriented dual control

$$\min_{\text{Input spectrum}} \quad \text{NE}[u_t^2], \quad \text{s.t. } \mathcal{I}_1^N(\theta_o) \succeq \frac{\gamma n}{2} V''_{\text{app}}(\theta_o)$$

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Policy: $\pi_t(x, u) = \mathbb{P}\{u_t = u \mid x_t = x\}$

Markov Decision Process formulation: Implementation

$$\begin{aligned} \min_{\pi} \quad & C_{\beta}(\pi) \\ \text{s.t.} \quad & \textcolor{red}{N}\mathcal{I}_{\beta}(\pi, \theta_o) \succeq \frac{\gamma n}{2} V''_{\text{app}}(\theta_o) \\ & x_t \in \mathcal{X} \subseteq \mathbf{R}^n, y_t \in \mathcal{Y} \subseteq R^p, u_t \in \mathcal{U} \subset \mathbf{R}^m \end{aligned}$$

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Occupancy measure

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MDP problem is a semi-definite program in $\{z_{xu}\}$.

Markov Decision Process formulation: Simulation study

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x split in 51 regions.

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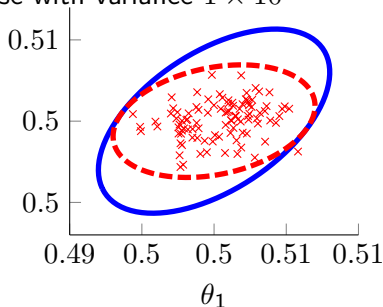
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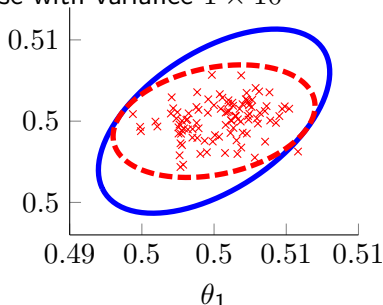
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Set of acceptable models: Blue solid ellipse.

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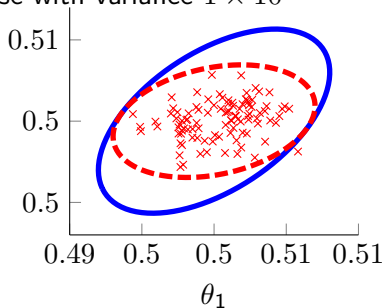
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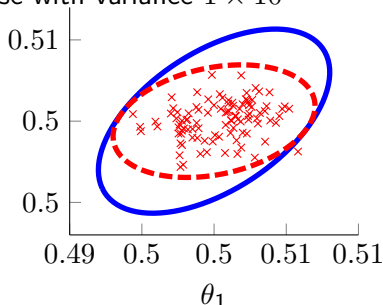
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Crosses: 100 Monte Carlo simulations using the MDP controller

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- Leads to a semi-definite program

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- but suffers from the curse of dimensionality due to discretization of state-space

Receding horizon formulation

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Cost at time t :

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Scaling κ_t monotonically increasing from 0 to 1 at $t = N - N_I$

Receding horizon formulation

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\Rightarrow Cannot use spectrum as design variable

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MPC-X: Model Predictive Control with eXperimental constraints

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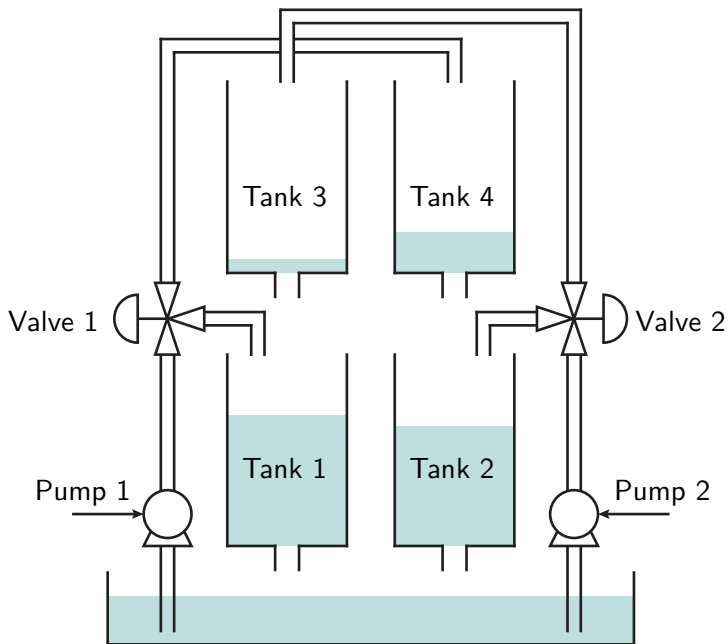
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Do not take application into account explicitly

Receding horizon formulation: Simulation study



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$$\left\{ \begin{array}{l} x_{t+1} = \begin{bmatrix} \theta_3 & \theta_4 \\ 1 & 0 \end{bmatrix} x_t + \begin{bmatrix} 4.5 \\ 0 \end{bmatrix} u_t, \end{array} \right.$$

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$$N = 200, \quad F = 5$$

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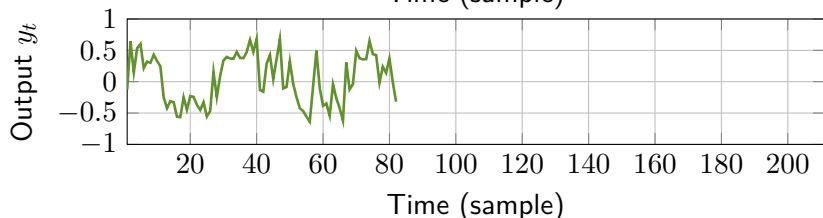
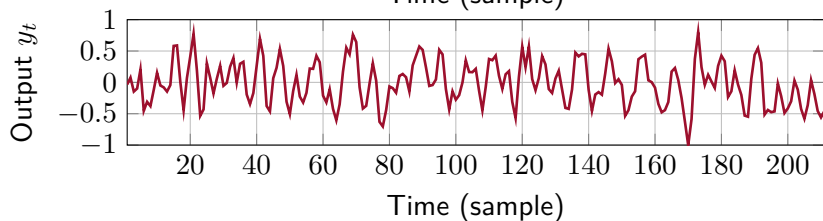
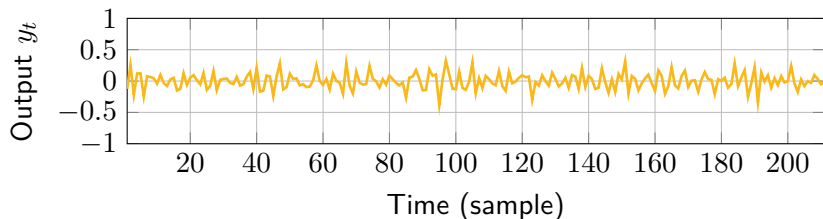
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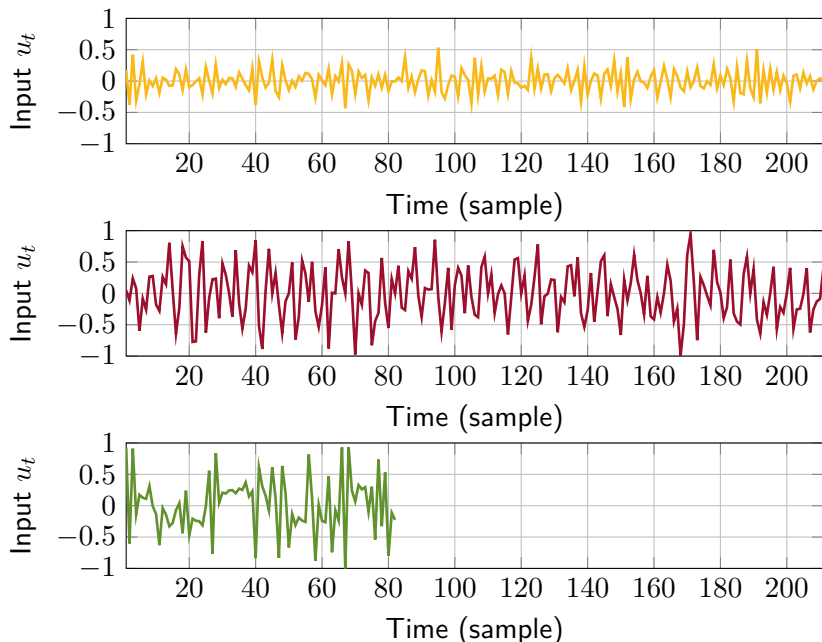
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MPC-X: Minimum time formulation

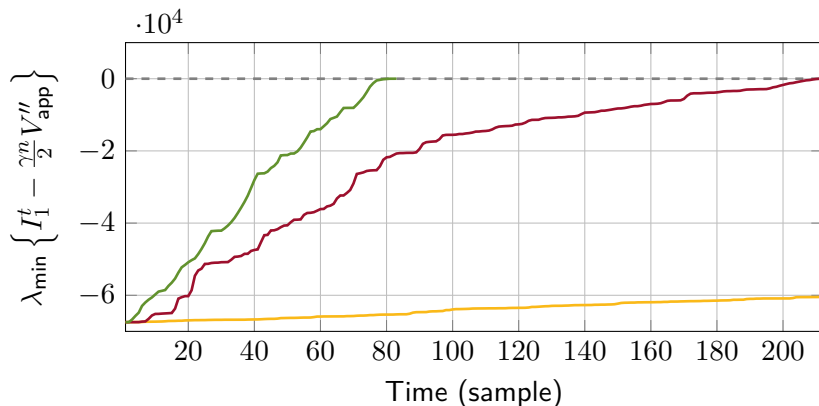
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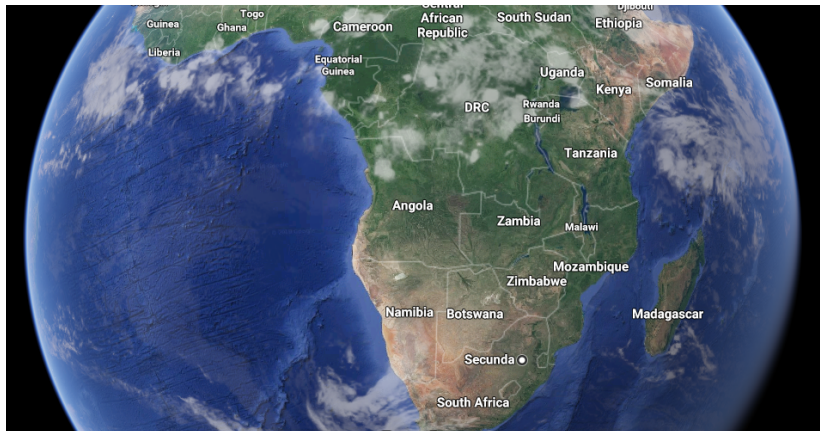


- Regular MPC (—),
- PE-MPC with $\rho = 0.5$ (—)
- Minimum time MPC-X (—)

Receding horizon formulation: Simulation study

Algorithm	Var u	Var y	N
MPC-X, minimum time	0.203	0.146	82
PE-MPC, $\rho = 0.5$	0.175	0.120	211

MPC-X experimental study: Let's travel



Secunda, South Africa



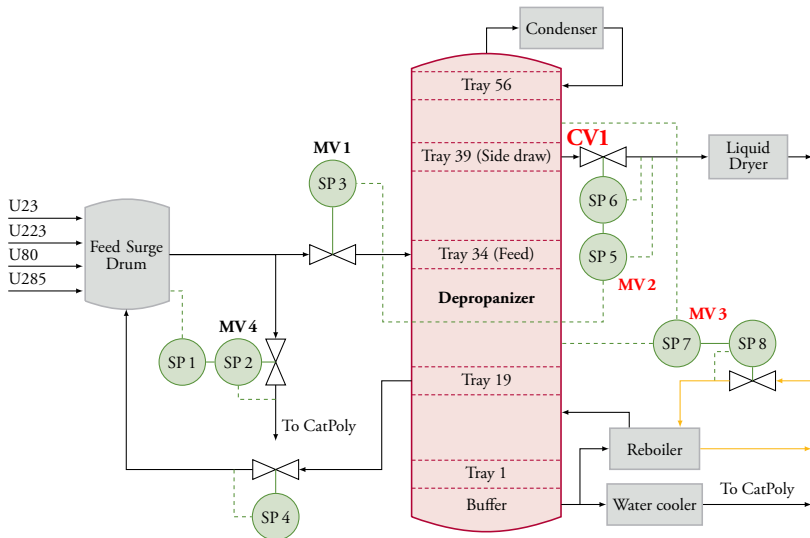
SASOL Synthetic Fuels Refinery



Synfuels Catalytic Cracker (SCC)



Depropanizer



Depropanizer

Separates three-carbon hydrocarbons (C_3) from four carbon hydrocarbons (C_4)

Objective: Set point for CV1= C_4 concentration in side draw

MV2: Side draw to feed ratio

MV3: Column differential pressure

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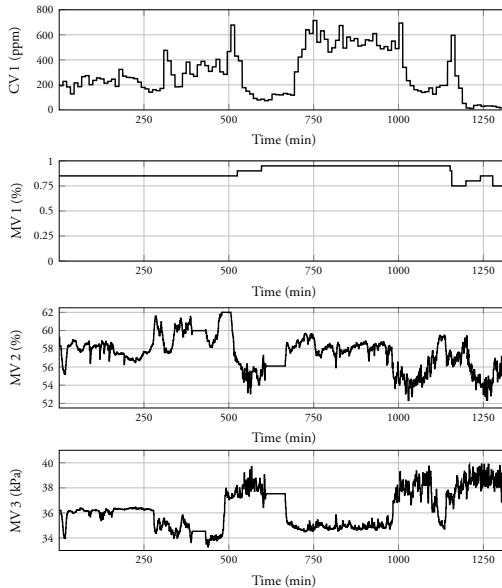
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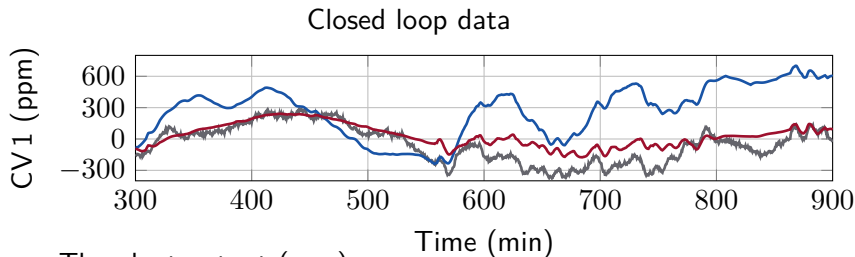
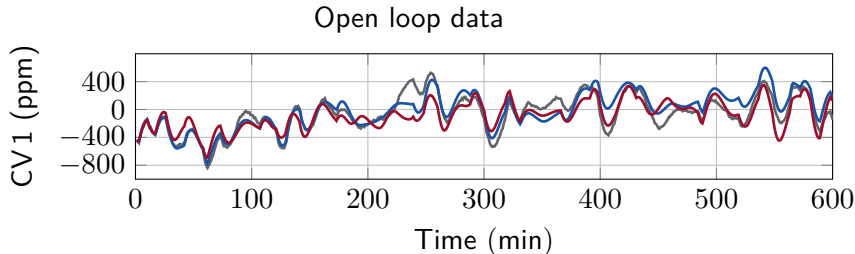
Performance drop obtained by changing poles of model

Excitation level manually controlled

Depropanizer: MPC-X experiment



Depropanizer: Model fit



- The plant output (—)
- Model identified in open-loop (—)
- Model identified in closed-loop MPC-X experiment (—)

Depropanizer: Closed loop performance

	Model	Variance	
		CV 1	MV 5
Before MPC-X		95×10^3	34×10^7
After MPC-X model update		36×10^3	37×10^7

MV 5 = C_4 content in the feed

MPC-X: Summary

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- Current limitation: Output error models (disturbances not modeled)

Outline

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Output error models

The impact of optimal experiments on the identification problem

Computing the optimal input

Experimental results

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- The optimal experiment matches the identification criterion to the performance degradation using parsimonious excitation
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- Simplifies the identification problem
- Active application oriented learning practical implementation
- Adding the Information Application Inequality to an optimal control problem leads to dual control

Acknowledgements

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THANK YOU!!!